

**AMENDMENTS TO THE SPECIFICATION**

Please amend paragraph 00051 as follows:

[00051] FIGURE 4 illustrates the flow diagram of the subject invention employing both the azeotropic distillation, with entrainers to form azeotropes and a steam generation/heat recovery system in the dehydration section of the terephthalic acid plant. The present invention further improves azeotropic distillation systems by generating steam during the separation of acetic acid from water in the distillation phase of terephthalic acid production. Isobutyl acetate (IBA) or normal butyl acetate (NBA) or their mixtures is used as an entrainer in the acetic acid dehydration column. The column has an overhead operating pressure of 1.3 kg/cm<sup>2</sup> abs. or higher. A steam generation system is located on top of the dehydration column to recover the steam energy by condensing the overhead vapor column. The steam is a low pressure steam of about 0.6 - 2.0 kg/cm<sup>2</sup> abs. In another embodiment, the steam is a low pressure steam from 0.7 - 2.0 kg/cm<sup>2</sup> abs. Acetic acid is recovered from the system in the amount of 300-800 ppm.